

NOVEL REACTOR WITH MULTIPLE ZINC ELECTRODES FOR SCALE PREVENTION

Marjana Simonič¹

¹*Faculty of Chemistry and Chemical Engineering, University of Maribor, Smetanova 17, Maribor, Slovenija
e-mail: marjana.simonic@um.si*

Abstract

The use of zinc reactor system with multiple electrodes was studied. Physico-chemical analyses of water and X-ray powder diffraction (XRD) of scale were performed without treatment and after the water passed through the reactor. The results showed that chemical parameters were remained the same after the treatment. Very small concentration of Zn²⁺ was detected in water after the treatment. The XRD analyses showed that in drinking water the share of calcite was higher, while only aragonite was formed after the treatment.

Introduction

Carbonate CaCO₃ precipitation in drinking water is a crystal mixture of calcite and aragonite at certain ratio between them. The share of calcite is affected by temperature, pH, ion concentration and suspended solids

In our previous study it was proved that Zn substantially inhibited the nucleation rate of CaCO₃ [1]. Crystallization of aragonite CaCO₃ was studied [2]. It was discovered that the morphology of carbonate precipitate differs a lot upon the crystal structure. Recently, a lot of efforts have been done to generate green inhibitors, either from plant extraction or by using natural organic molecules. [3] However, it is complicated if chemicals are added directly into the water and could affect the chemical water quality.

The main objective of the present research, was to study the effect of reactor with multiple Zn electrode on scaling and CaCO₃ crystal morphology was studied. The calcite/aragonite ratio was studied by means of a chemical analysis and X-ray powder diffraction. A mechanism has been proposed that the surface reaction of Zn-ions with CaCO₃ might be rate determining step in the crystallization process.

Experimental

Untreated water samples were taken from waterworks (Maribor, Slovenia). Water flowed through the Zn-reactor (Figure 1) directly from the water pipe. The sample was taken at the outflow from the reactor. Samples of untreated and treated waters were saved for chemical and XRD analyses.

The device in Figure 1 operates due to certain potential difference which is governing the process of scale prevention. Inside the reactor there are multiple zinc electrodes as seen from Figure 1. Due to potential difference the device inhibits the scale formation. For the proper working the ratio between zinc versus copper electrode area (S_{zn}/S_{cu}) is very important.

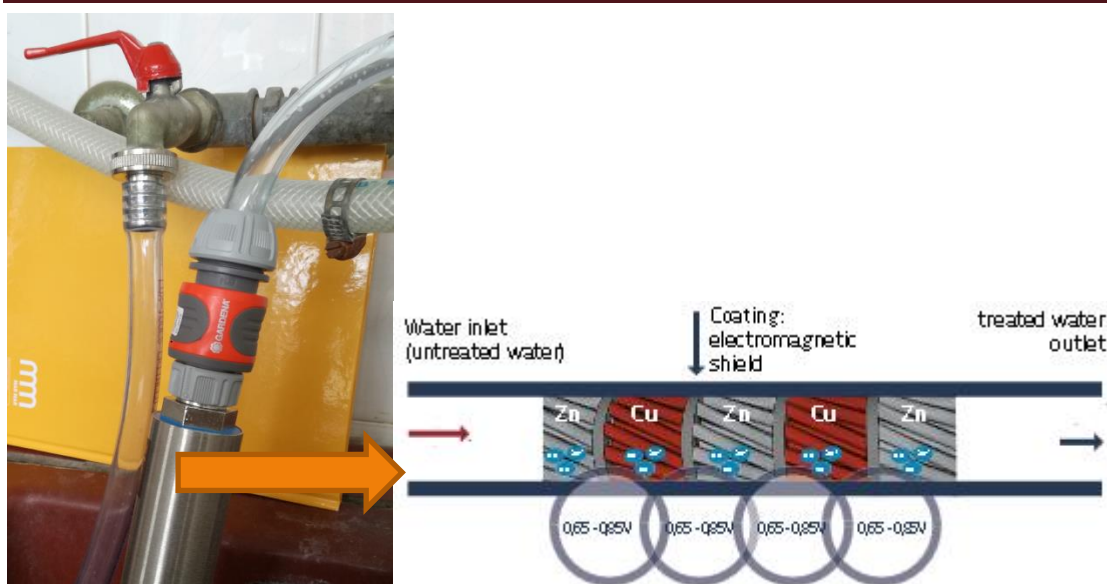


Figure 1. Zinc reactor

The chemical analysis of water was made in three replicates. The standard methods are gathered in Table 1.

Table 1. The methods used for water analyses

| Parameter | Standard method | Apparatus |
|------------------------------|----------------------|-------------------------------|
| T (°C) | ISO 10523 | Thermometer |
| pH | ISO 10523 | pH-meter, MA 5740 |
| TH (°d) | 38409-H6 (1986) | Titration |
| Ca^{2+} , Mg^{2+} (mg/L) | 38406-E3 (1982) | Titration |
| Zn^{2+} , Cu^{2+} (µg/L) | ISO DIN 11885 (1993) | ICP-MS/Perkin Elmer Elan 6000 |

X-ray powder diffraction data were collected with an AXS-Bruker/Siemens/D5005 diffractometer, using Cu-K α radiation at 293 K. The samples were scanned with positin sensitive detector and measured in range $10^\circ < 2\theta < 80$, with the step of 0,01 and scanning speed of 2 s per step. Determination of phases in the sampe was done with Search/Match program.

Results and discussion

Water was taken after passing through the Zinc reactor. Results of chemical analyses are shown in Table 2.

All experiments were performed at room temperature.

Table 2. The methods used for water analyses

| Analysis | Drinking water | Treated water |
|-------------------------|----------------|---------------|
| T(°C) | 20 | 20 |
| Ca ²⁺ (mg/L) | 65,7 | 65,7 |
| Mg ²⁺ (mg/L) | 21,3 | 21,3 |
| Zn ²⁺ (mg/L) | < 0,01 | < 0,01 |
| Cu ²⁺ (mg/L) | <0,01 | <0,01 |
| TH (°d) | 14,1 | 14,1 |

It is clearly seen that chemical water quality remained the same after the treatment. Also none of the Zn concentration difference was noted. Copper concentration was also measured due to the content of the reactor. The concentration in drinking water was below 10 µg/L.

XRD analysis of scale formed in untreated water and in treated water was performed. The diffractogram of the precipitate from untreated water showed some calcite crystals peaks (denoted C in Figure 1a). Zinc reactor device induced changes to the crystal morphology and promoted crystallization in the aragonite rather than calcite. Only aragonite in powdered form was formed after the treatment (Figure 1b).

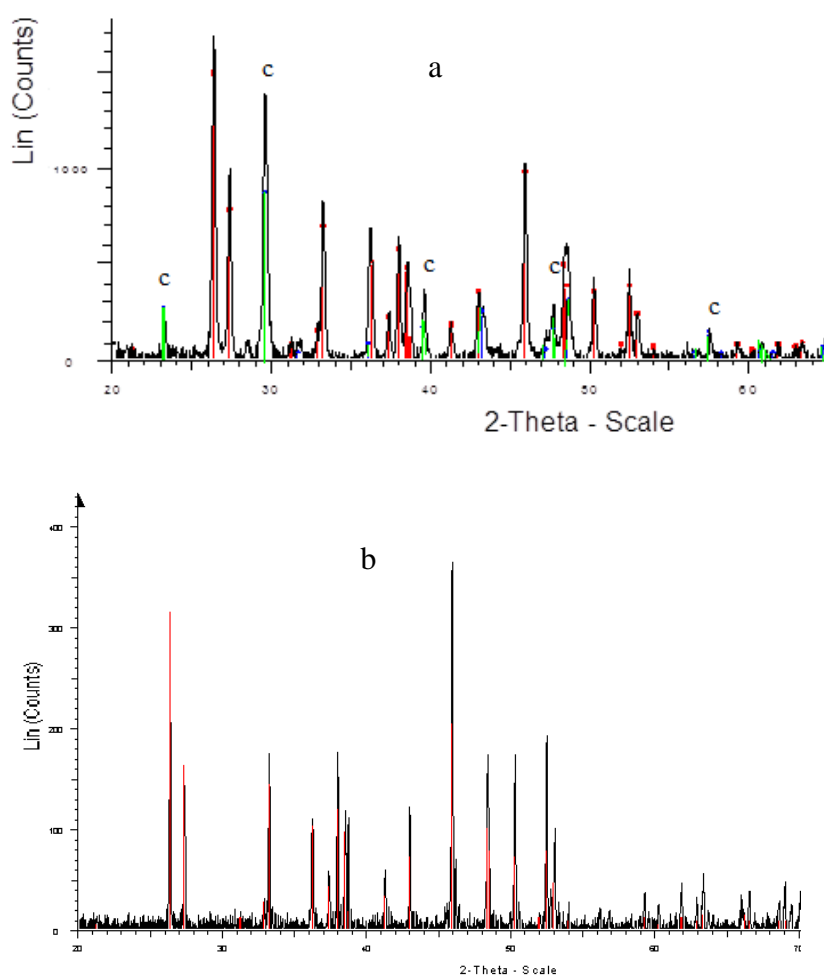


Figure 2. XRD analysis of CaCO₃ (a pattern denotes the untreated water, b treated water)

Since the product is novel, the operating time of reactor could be estimated at 10 years according to the results. Due to calcite formation inhibition the pipes are preserved and there is prolonged the lifetime of pipes. Further, no chemical cleaning is needed for scale removal inside the entire water pipeline system. Therefore, device minimizes operational costs.

Conclusion

The trace amounts of Zn substantially inhibit the nucleation rate of calcium calcite. The Zinc concentrations below 10 µg/L enable the formation of aragonite and disable the formation of calcite. Already after analyses of the scale it was found the powdered form of aragonite was formed.

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